3	In situ microwave assisted extraction of clove buds to isolate essential oil,
4	polyphenols, and lignocellulosic compounds
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17 ABSTRACT

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Clove buds is a spice of relevance in food, traditional medicine, pharmaceutics and cosmetics and, among 19 the spices, they have the highest content of total polyphenols with exceptional antiviral and antimicrobial 20 properties. Various approaches have been reported for the isolation of essential oil from clove buds. 21 22 Nonetheless, the qualitative and quantitative analysis of hydrosoluble polyphenols and solid residues simultaneously yielded during the extraction process has not been explored yet. This work is focused on 23 the analysis of some variables effect on yield and composition of the clove buds essential oils on a green 24 microwave assisted extraction, and the characterization and quantification of the different compounds 25 obtained from the extraction process. A versatile coaxial dipole antenna, to directly apply the 26 electromagnetic energy inside the extraction medium, was used to thermally activate the hydrodistillation. 27 28 The composition profiles of clove buds essential oil and hydrosoluble polyphenols obtained during in-situ microwave assisted extraction (IMWAE) were analysed and quantified by head space gas chromatography 29 mass spectrometry (HS-GC-MS) and liquid chromatography with UV/visible diode array/fluorescence 30 31 detector (HPLC-DAD-FD). The solid residue was characterized by Fourier Transform Infrared (FTIR) spectroscopy and its composition in term of lignin, cellulose and hemicellulose was predicted. The green 32 33 IMWAE process was compared with the conventional hydrodistillation (CH) in terms of yield and quality of isolated products. Thermogravimetry coupled to FTIR analyses of the evolved gases from the solid 34 35 residue evidenced that the solid residue obtained from IMWAE of clove buds is richer in cellulosehemicellulose than the residue obtained from CH. This can be because of microwaves that allow to remove 36 37 a higher amount of phenolic compounds/lignin oligomers. The enthalpy of combustion values (Δ_c H) (kJ/g) of IMWAE and CH residues were determined by calorimetric combustion and were compared with the -38 $\Delta_{\rm c}$ H (kJ/g) values calculated using the hemicellulose, cellulose and lignin compositions predicted by partial 39 least square chemometrics. The Δ_{c} H highlighted the energetic features of solid residues from IMWAE and 40 CH for their potential uses as alternative biomass for fuel production and here firstly reported for this kind 41 42 of biomass. The extraction approach here presented is environmentally friendly, highly flexible, easily controllable, time saving, and enables to break the scale-up barrier in microwave assisted industrial 43 processes aimed to valorise aromatic herbs and eventually to exploit vegetable wasting materials. This 44 45 leads to a lowering of production costs and, therefore, of the market price of isolated extracts from aromatic herbs. 46

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Keywords: Biomass Food chemistry • Clove buds • Microwave chemistry • Polyphenols • Renewable
resources

50 Introduction

51 Aromatic herbs, medicinal plants and lignocellulose biomass represent one of the most fascinating new platforms for biorefinery, which allows the extraction of an unlimited amount of different chemical 52 compounds to be used as bioactive compounds for specific applications such as fragrances, personal care 53 products, medicines or fuels for green energy production (Zuin et al., 2018). Most of the time, the efforts 54 were focused on a one-target product isolation approach, such as for essential oils extraction (EOs). 55 However, this approach leads to an increase in the costs and environmental impact of isolated products. 56 EOs extracted from aromatic herbs are, indeed, expensive products due to their intrinsic low extraction 57 58 yield and cost of their production. These complex mixtures of volatile organic compounds have been typically isolated by steam distillation (Schimdt, 2010). 59

60 Classical hydrodistillation (CH) was developed at lab scale as a simple extraction approach involving only 61 water, herbs and energy (Rassem et al., 2016; Schimdt, 2010). Thus, the efforts to optimize this extraction 62 process to isolate EOs were focused on the minimization of energy consumption, time and cost of the 63 process.

Hydrodistillation has been then enhanced by the use of various energy sources and environmentally friendly 64 65 extraction methods like microwave assisted extraction (MWAE) (Bagherian et al., 2011; Golmakani and Rezaei, 2008; Gonzalez-Rivera et al., 2016; Gonzalez Rivera et al., 2016; Roldán-Gutiérrez et al., 2008; 66 67 Saleh et al., 2016; Tiwari, 2015), supercritical fluid extraction (SFE) (Cassiana Frohlich et al., 2019) and ultrasound-assisted extraction (Pingret et al., 2014; Roldán-Gutiérrez et al., 2008; Saleh et al., 2016). Green 68 69 solvents like ionic liquids have been also tested (Ascrizzi et al., 2017). These methods have been shown suitable to produce EOs with sensorial properties similar to those obtained by CH, with the advantage in 70 71 term of costs and timesaving.

The yield and chemical composition of the extracts depend on the extraction method employed for EOs 72 73 isolation and the intrinsic properties of the plant (Ascrizzi et al., 2017). Considering the target of obtaining high quality and high purity EOs, significant amounts of solid residues are also produced as by-products. 74 75 These solid residues are mainly condensate polyphenols or insoluble cellulosic materials (Santana-Méridas et al., 2014), which can be used as biomass precursors to obtain energy or bio-compound derivatives. In 76 EO hydrodistillation, high amounts of condensed water (also named as herbal water or hydrosol) containing 77 non-volatile soluble bioactive compounds with strong antioxidant properties (hydrosoluble polyphenols, 78 proteins/enzymes, aminoacids, polysaccharides, alkaloids, alcoholic compounds and vitamins) are also 79 80 produced (Petigny et al., 2014).

Polyphenols, in particular, have been found to have a strong antimicrobial and antiviral activity (Chiow et al., 2016; de Oliveira et al., 2015; Jassim and Naji, 2003; Mukhtar et al., 2008; Song et al., 2005; Zhang et al., 2020; Zhong et al., 2012). Oleuropein (Omar, 2010), for example, and its derivatives (tyrosol and hydroxytyrosol) (Yamada et al., 2009) (extracted from olive leaves, *Olea europaea*) and eugenol (extracted from cloves, *Eugenia caryophyllus L.*) (Hume, 1986) have a structure similar to the conserved amino acids of the SARS-COV-19 virus S protein involved in receptor interaction (Sivanesam and Andersen, 2019).

Hydrodistillation offer a clear opportunity to valorize by-products. This work aims to investigate the effects 87 of several variables on yield and composition of the clove buds EO and their by-products (polyphenols and 88 lignocellulose) using a microwave assisted hydrodistillation process with microwave energy applied *in situ* 89 90 (*in situ* microwave assisted extraction, IMWAE) (Figure 1). This approach is based on the uses of a coaxial dipole antenna to directly apply the electromagnetic energy inside the extraction medium (Calinescu et al., 91 92 2017; Longo and Ricci, 2007). IMWAE has been previously successfully applied to the extraction of EO from lavender, sage, rosemary, fennel seed and clove buds (Gonzalez Rivera et al., 2016). IMWAE features 93 a series of advantages: i) it easily provides microwave energy in a reaction vessel getting rid of the 94 restrictions of having a defined closed metal cavity, ii) it avoids the dispersion of the radiation since all the 95 energy generated by the magnetron is absorbed by the sample providing very high energy density and, iii) 96 the reactor walls can be made of any material and geometry. Moreover, the reactor can be safely installed 97 in every kind of research laboratories or industrial environments. Conventional hydrodistillation was also 98 investigated as comparison. 99

100

101 Figure 1

102

Clove buds have been chosen in this study as ligneous, representative substrate due to its relevance in food, 103 104 traditional medicine, pharmaceutics and cosmetics (Khalil et al., 2017). Cloves are the aromatic flower buds of a tree in the family Myrtaceae, Eugenia caryophyllus, native to the Maluku Islands in Indonesia, 105 and mainly used as a spice. Cloves are commercially harvested primarily in India, Pakistan, Indonesia, 106 Madagascar, Zanzibar, Sri Lanka and Tanzania. But, Indonesia and Madagascar are the main clove buds 107 oil producer (Uddin et al., 2017). Oil is extacted from buds, leaf and stem oil. Bud oil contains 60-90% 108 eugenol, the main component, eugenyl acetate, caryophyllene and other minor constituents (Cortés-Rojas 109 et al., 2014). Several reports highlighted that the daily intake of cloves can help to control the glucose, 110

triglycerides and LDL cholesterol levels in the blood (Khan et al., 2006) and that clove buds are among the
spices with the highest content of total polyphenols (Assefa et al., 2018).

The strong antimicrobial, antifungal, anti-inflammatory and antiviral activity of eugenol emerged from a 113 114 number of recent studies (Marchese et al., 2017). Specifically, eugenol has shown promising antiviral activity against feline calicivirus, tomato yellow leaf curl virus, influenza A virus, herpes simplex virus 115 type 1, herpes simplex virus 2, ebola virus, four airborne phages as well as larvicidal activity against Aedes 116 aegypti (Lane et al., 2019) and references therein), anesthetic activity, inhibitory activity towards the 117 pathogens of dental caries (Uju and Obioma, 2011), antioxidant potential, antimicrobial role (Hadidi et al., 118 2020), antifungal role (Munoz Castellanos et al., 2020; Wan et al., 2020), anti-inflammatory action, anti-119 120 carcinogenic effects (Nirmala et al., 2019), neuroprotective ability, hypolipidemic efficiency and antidiabetic effectiveness (Gonzalez Rivera et al., 2016; Grumezescu et al., 2013; Lee and Shibamoto, 2001). 121 122 Studies showed that eugenol inhibits the replication of influenza A virus by interfering with the ERK, p38MAPK and IKK/NF-κB signal pathways (Dai et al., 2013). Eugenol has a structure similar to conserved 123 amino acids in the sequence of spike protein (S protein) of SARS-CoV-2, which is involved in the 124 interaction with ACE2 receptors during infection (Sivanesam and Andersen, 2019). It is reasonable to 125 hypothesize that the interaction of eugenol or other similar small polyphenols may interact with beta 126 structures of S protein avoiding the attack of the virus to the host cell (Bramanti et al., 2013, 2010; 127 Sgarbossa et al., 2013). Eugenol is generally recognized as a safe and non-mutagenic compound by World 128 Health Organization ("TOXNET. Toxycologycal data network: Eugenol," n.d.). Novel application of clove 129 EO includes its use as a green monomer to produce polymers (Deng et al., 2015). 130

Clove bud polyphenols have a powerful antimicrobial and antiviral activity (Chiow et al., 2016; de Oliveira et al., 2015; Jassim and Naji, 2003; Mukhtar et al., 2008; Song et al., 2005; Zhang et al., 2020; Zhong et al., 2012). Among these, quercetin has been found have a potential role against coronavirus disease 2019 (COVID-19) (Derosa et al., 2020). In several applications polyphenols have been used to treat materials in order to give them antiviral properties (Catel-Ferreira et al., 2015; Kazuo and Yoshikatzu, 1997).

In view of the properties mentioned above, in this work IMWAE has been applied to clove buds (i) as representative, complex, ligneous matrix, (ii) in order to chemically characterize not only EO, but also residual condensed water and solid residue after IMWAE and CH. While many extraction approaches have been addressed only to optimize the yield of clove EOs, few information are reported in the literature on the chemical composition of by-products. EO composition has been assessed using headspace gas chromatography mass spectrometry (HS-GC-MS). The polyphenolic profile of water extracts has been assessed by liquid chromatography with UV/visible diode array and fluorescence detector (HPLC-DAD-

FD). The solid residue obtained after IMWAE and CH has been characterized by thermogravimetric 143 analysis coupled to FTIR (TGA-FTIR), ATR-FTIR and by calorimetric combustion. TGA-FTIR has 144 allowed us to investigate the thermal behaviour and the composition of the gases evolved during the thermal 145 decomposition of the solid residues after both IMWAE and CH of clove buds. FTIR spectroscopy coupled 146 to partial least squares (PLS) analysis has allowed us to quantify the lignin, cellulose and hemicellulose 147 content of solid residue by applying a chemometric method previously developed (Chen et al., 2010). 148 Enthalpy of combustion values ($\Delta_c H$) was also calculated based on the calorimetric combustion of IMWAE 149 and CH. This information, which is reported here for the first time, is potentially useful for the alternative 150 uses of these solid residues as fuels for energy production. 151

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153 Experimental

154 Materials

Dry clove buds (Indonesia) were purchased from a local market. Phloretin, ellagic acid, resveratrol, 155 chlorogenic acid, cyanin chloride, coumarin, quercetin, tannic acid, resorcinol, pyrocatechol, pyrogallol, 156 (-)-epicatechin, gallic acid, (-)-epigallocatechin gallate, rosmarinic acid, trans-ferulic acid, caffeic acid, 157 1,3,5-trihydroxybenzene dehydrate, salicylic acid, acetylsalicylic acid, (+)-abscisic acid, vanillin, 158 pinoresinol, (+)-catechin and eugenol were HPLC analytical standards purchased from Merck (Milan, 159 Italy). Tyrosol, hydroxytyrosol, oleuropein, syringic acid, luteolin and apigenin were purchased from 160 Extrasynthese (Cedex, France). Deionized water obtained with a Milli-Q system (Purelab Pro + Purelab 161 Classic, Millipore, USA) was used as a solvent for all the extractions. Ethanol (EtOH for HPLC, $\geq 99,8\%$, 162 Fluka), methanol (MeOH for HPLC >99%, Merck), dimethyl sulfoxide (DMSO for GC >99,5%, Merck), 163 sodium hydroxide (NaOH 0.1 M, Merck) and formic acid (~98%, Fluka) were used as solvents for the 164 preparation of standards solution of polyphenols. 165

166

167 In situ microwave assisted extraction (IMWAE)

The IMWAE apparatus, experimental set-up and extraction procedure are described as follow based on our previous works with slight modifications (Gonzalez Rivera et al., 2016). Dry clove buds were ground to a fine powder using a laboratory blender. A weighted amount (5, 10 or 20 g) of grounded clove buds was mixed with 200 mL of deionized water and the aqueous substrate dispersion was loaded into a 350 mL flask vessel. The vessel was wrapped by a metallic grid to prevent the emission of MW irradiation out of the

reaction medium and to ensure safe operating conditions. MW energy was applied by means of a coaxial 173 dipole antenna immersed into the extraction medium, protected by a glass tube. The extraction medium was 174 heated in the MW assisted device, for 10 min using 150 W of MW power while continuously stirring the 175 mixture at 250 rpm. The source of microwave was a magnetron oscillator equipped with forward and 176 reflected power indicators (SAIREM, Mod. GMP 03 K/SM, up to 300 W of continuous MW irradiation 177 power at a frequency of 2.45 GHz). Once the hydrodistillation had started, the power was kept at 150 W 178 for 90 min under steady state conditions. The extraction time has been selected based on literature reports 179 and previous published data of clove bud extraction by coaxial microwave assisted hydrodistillation 180 (Gonzalez Rivera et al., 2016). After completion of the extraction process, the EO was collected, decanted, 181 dried and weighed. The condensed water remained in the flask vessel was separated from the solid clove 182 bud residue by 12 min centrifugation at 5000 RPM. EO and condensed water were stored at 4 °C and -20 183 °C, respectively, in dark containers for further HS-GC-MS and HPLC-DAD-FD characterization. The 184 condensed water after extraction, also known as hydrosol, or herbal water corresponds to the total volume 185 of water used for the hydrodistillation. The concentration of water-soluble polyphenols hence corresponds 186 to the total amount of water used for the extraction. The solid residues were dried at 60 °C overnight before 187 FTIR and TGA-FTIR. Deionized water has been employed in this work for analytical purposes of the 188 189 products. For the scale up in industrial processes any type of water can be employed depending on the subsequent use of the products. 190

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192 EO extraction by conventional hydrodistillation (CH)

Hydrodistillation of clove buds using conventional heating was also performed for comparison. Briefly, 5 g of ground clove buds were loaded together with 200 mL of deionized water in a typical Clevenger extractor. The extraction was thermally activated using a standard electric mantle operating at 250 W. Both IMWAE and CH processes have been operated at 100°C. This detail has been added in the experimental.

197

198 HPLC-DAD-FD analysis

Condensed water extracts were analyzed using HPLC-DAD-FD system. An HPLC gradient pump (P4000,
ThermoFinnigan) was coupled with a vacuum membrane degasser (SCM1000, ThermoFinnigan), an
AS3000 autosampler (ThermoFinnigan), a UV6000 diode array detector and a FL3000 fluorescence
detector (ThermoFinnigan). Separations of polyphenols were carried out using a reversed-phase HPLC

- column C18 Spherisorb S5 ODS2 (Waters, 250 mm x 4 mm, 5 μm). Column temperature was set at 40 °C
 and injection volume was 20 μL.
- Mobile phases for the determination of polyphenols in standard solutions and condensate water samples was 5% methanol–0.1% formic acid in water (eluent A) and 95% methanol-0.1% formic acid in water (eluent B). The gradient was as follows: 0–5 min, 100% A; 5–45 min, linear gradient up to 100% B; 45–55 min 100% B; 55–57 min, linear gradient up to 100% A. Post-run time was 15 min. Elution was performed at a solvent flow rate of 0.8 mL min–1. Table S1 summarized the retention time (t_R), solvent used for stock solution preparation and spectra information (UV absorbance (λ_{max}) and fluorescence ($\lambda_{excitation}/\lambda_{emission}$)) of 31 polyphenols standards separated using the above conditions.
- ChromQuestTM 4.2 Chromatography Data System was used to carry out HPLC-DAD/FD control, data
 acquisition and data analysis.
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215 Headspace gas chromatography/ mass spectroscopy (HS-GC-MS)

- Clove bud essential oils were analysed by HS-GC-MS. The analysis was carried out using an Agilent 6850 gas chromatograph coupled with an Agilent 5975c mass spectrometer. An Agilent GC Sampler 80 was employed for HS sampling. The vials were incubated at 80 °C for 15 min. The chromatographic separation was carried out on a J&W DB-WAX Ultra Inert column, ($60 \text{ m} \times 0.25 \text{ mm}$, $0.5 \mu \text{m}$ film thickness) supplied by Agilent Technologies (USA). Helium 5.6 IP was used as a carrier gas at constant flow of 1 mL/min. The oven temperature program was as follows: 40 °C for 5 min, 19 °C/min up to 230 °C. The total runtime was 58 min. The temperature of the transfer line and ion source was set at 240 and 250 °C, respectively.
- 223

224 ATR-FTIR spectroscopy analysis

- Infrared spectra were recorded by using a Perkin-Elmer Spectrum One FTIR Spectrophotometer, equipped
 with a universal attenuated total reflectance (ATR) accessory and a triglycine sulfate TGS detector.
 Measurements were performed in attenuated total reflectance (ATR) mode after background acquisition.
 For each sample, 32 scans were recorded, averaged and Fourier-transformed to produce a spectrum with a
 nominal resolution of 4 cm⁻¹.
- 230

231 Thermogravimetric- Fourier-transform infrared spectroscopy analysis (TG-FTIR)

The thermogravimetric experiments were performed using a TA Instruments Thermobalance model 232 Q5000IR equipped with an FTIR Agilent Technologies spectrophotometer model Cary 640 for Evolved 233 234 Gas Analysis (EGA). TG-FTIR measurements were performed using Pt crucibles at a rate of 20 °C/min, from 30 °C to 900 °C under air or nitrogen flow (80 mL/min). The amount of sample in each measurement 235 varied between 10 and 15 mg. Mass calibration was performed using certified mass standards, in the 0–100 236 mg range, supplied by TA Instruments. The temperature calibration was based on the Curie Point of 237 paramagnetic metals. TG-FTIR measurements were performed in the range 600–4000 cm⁻¹ with a 4 cm⁻¹ 238 width slit. To reduce the strong background absorption from water and carbon dioxide present in the 239 240 atmosphere in the TG-FTIR spectra, the optical bench was usually purged with nitrogen. In addition, a background spectrum was taken before the beginning of each analysis in order to zero the signal in the gas 241 242 cell and to eliminate any contribution from ambient water and carbon dioxide.

243

244 Combustion calorimetry

Combustion of biomass samples was carried out by a home-made bomb calorimeter. A standard stainless-245 steel bomb (volume = 375 ml) is placed in a bath with 2200 ml of water, equipped with a stirring system 246 and a temperature probe (thermistor). The bath is lodged in an isoperibol calorimeter. The calorimetric 247 curves are acquired by a personal computer and corrected to account for the heat losses through the 248 calorimetric wall. The calorimeter was previously calibrated by benzoic acid certified standard. One gram 249 250 of sample was pressed to form a pellet and placed in a crucible with about 0.5 g of hexadecane. An iron wire was then immersed in the hexadecane and connected to electrical terminals. Then, about 0.5 ml of 251 water where placed in the bottom of the bomb in order to saturate the vapor phase of water and get the 252 higher calorific value of the sample. Finally, the bomb was closed and pressurized with oxygen (99.9%, 25 253 bar) after flushing for about 30 seconds, placed in the calorimeter and the sample was ignited. The ΔU value 254 was obtained for each experiment from the thermal effect, corrected for the heat losses. The blank 255 contribution due to the combustion of the ignition wire and hexadecane was subtracted. The experiments 256 were carried out at 25 ± 0.1 °C. The enthalpy of combustion can be obtained by Eq. (1): 257

258 $\Delta_c H(p,T) = \Delta_c U(p,T) + \Delta v_a RT \quad (1)$

where Δv_g is the variation of number of moles of gaseous species due to the combustion. However, since $\Delta v_g = 0$ for both cellulose and hemicellulose, only the contribution due to lignin combustion should be

- considered. Considering that the molar fraction of lignin in the biomasses here analysed is between 0.15 and 0.26, the correction term to calculate $\Delta_c H$ from $\Delta_c U$ is between -0.003 and -0.005 kJ g⁻¹, which is within the experimental error. The correction for pressure value, $p \neq 1$ bar, is neglectable, as well. The overall uncertainty on the $\Delta_c H$ values is within $\pm 2\%$ (N=3).
- 265

266 **Results and discussion**

267 Clove buds essential oil yield and composition

Clove buds are well known attractive substrate due to their high EO content and low cost. The maximum amount of clove EO that can be extracted depends on their geographical origin of production, on the part of the plant used for their extraction (leaves, buds or mixture thereof), on the pre-extraction treatment and the extraction method employed. Figure 2 (a) shows the yield percent of clove buds EO isolated by IMWAE using different liquid to solid ratio (L/S_{ratio}=10, 20 and 40) and fixed MW extraction conditions (reflux of water using 150 W of MW at 2.54 GHz).

High EO extraction yields ranging from 5.5 ± 0.8 up to $16\pm1.5\%$ were obtained after 90 min of IMWAE. The EO yield % strongly depends on the liquid to solid ratio, achieving the highest value at the highest ratio explored. Figure 2 shows also the clove buds EO yield % obtained by CH as comparison. The extraction of EO by CH was performed using the best liquid to solid ratio value explored (L/S_{ratio}=40) used for the IMWAE. Under such conditions, CH yielded lower EO amount (7.8±0.8% wt) even if the extraction time used was more than 30% longer (120 min). Thus, IMWAE confirmed its advantages as faster and greener approach than CH, yielding higher amount of EO, as previously observed (Gonzalez Rivera et al., 2016).

281

282 **Figure 2**

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Table 1 summarizes the literature reports concerning the isolation of clove buds extracts by different approaches. EO yield values (widely ranging from 2.4 up to 41.8%) depend on both the extraction conditions (time, L/S_{ratio} and solvent) and the extraction approach used. The comparison between the different approaches (to maximize the yield %) is difficult since the clove bud cultivar and geographical origin are also important factors.

As general remarks, according to Table 1 standard, conventional hydrodistillations (Chin this work) and 289 steam distillation (SD) methods using water as solvent and the longest extraction times (from 120 to 360 290 min and from 240 to 600 min for CH and SD, respectively) reach yields below 10% (wt) if the L/Sratio is 291 below 1:10 (w/w) (Gonzalez Rivera et al., 2016)(Leon-méndez et al., 2018) (Guan et al., 2007) and up to 292 20% (wt) if the L/Sratio increases up to 1:20 (Clifford et al., 1999) (Kapadiya et al., 2018). MW assisted 293 extraction methods (IMWAE, MAE, MASE and MWHD) slightly increase the EO yields strongly 294 decreasing the extraction times (from 30 to 120 min) (Gonzalez Rivera et al., 2016) (Kapadiya et al., 2018) 295 (Golmakani et al., 2017)(Leon-méndez et al., 2018). 296

The highest yield (up to 41.8%) (Guan et al., 2007; Yang et al., 2014) was obtained using Soxhlet extraction 297 (SE) and ethanol for 360 min. These features and the need of an additional step to separate the solvent from 298 EO, make solvent approach unfavorable for environmental and economic reasons. Supercritical fluid 299 extraction (SFE) has become a popular approach for treatment of clove buds, achieving high yields (Clifford 300 et al., 1999; Guan et al., 2007; Reverchon and Marrone, 1997; Scopel et al., 2014; Yang et al., 2014). 301 However, high pressure processing (from 100 up to 200 bar) and long extraction times (from 110 up to 330 302 min) can considerable influence the cost of EO production, beside the intrinsic concerns in the safety of the 303 process due to high pressures involved. 304

Ultrasound assisted extraction (UAE) is a green approach and high EO yields (up to 41%) are obtained in short extraction time (45 min) (Alexandru et al., 2013; Tekin et al., 2015). The EO yields enhancement using UAE is related to the US negative pressure cavitation effects. The cell membranes of the substrate are disrupted by the hammer-like action of the produced solvent jets. However, this approach still uses organic solvents or water-organic solvent mixtures that require an additional step of separation of the organic solvent.

The IMWAE proposed in this work presents relative short extraction times (90 min) at atmospheric pressure, it uses only water as solvent, and it gives yields up to 16% EO without additional purification steps. Further benefits of IMWAE deal with an easy scale up, flexible technology, environmentally friendly approach, safe operations, and low cost.

Figure 2 (b) shows the chemical composition, expressed as percentage, of EO isolated from clove buds using IMWAE and CH, as comparison. Five compounds were identified by HS-GC-MS analysis, corresponding to the full EO characterization. Eugenol was the main compound (48.9±2.5 %) followed by β -caryophyllene (42.8±2.1 %). These two compounds account for more than 90% of EO composition. Other identified compounds were α -caryophyllene (3.7±0.2 %), α -cubebene (2.3±0.1 %) and α -copaene (2.2±0.1 %). The chemical composition of clove buds EO isolated through IMWAE or CH resulted statistically indistinguishable.

Table 1 also enlists the main compounds of clove EO extracted using clove buds from different 322 geographical sources, different approaches and extraction conditions. Despite the many diverse factors 323 involved during extraction, eugenol was the most abundant compound in all cases, with the exception of 324 UAE procedure (Alexandru et al., 2013) where α-humulene was reported as the main compound obtained 325 from various clove buds from China, India and Madagascar. β-caryophyllene and eugenyl acetate were also 326 observed in clove buds EO almost in all cases, particularly in EO from clove buds from China and India 327 (Table 1). Their composition, however, is more linked to the cultivar of buds used. EO extracted in this 328 work from Indonesia clove buds have 42.8 ± 2.1 % of β -caryophyllene while eugenyl acetate was not 329 detected. 330

 β -caryophyllene has been recently widely investigated due to its potential properties in biomedical applications as anti-carcinogenic (Fidyt et al., 2016) and organoprotective agent like the phytocannabinoids (Al-taee et al., 2019).

334

335 **Table 1**

336

337 Quantitative and qualitative analysis of hydrosoluble polyphenols

Figure 3 shows the HPLC-DAD (a) and FD chromatograms (b) of condensed water obtained after EO extraction by IMWAE and CH using a L/S_{ratio}=40 and, 90 min and 120 min of extraction time, respectively. Nine different main polyphenols were identified by the comparison of both UV absorbance/fluorescence spectra and retention time (t_R) of their corresponding analytical standards. To this purpose, an HPLC-DAD-FD method using 31 analytical standards was developed; eluent conditions, instrumentation, and polyphenols used in this work (including t_R and spectra information, λ_{max}) are fully described at the experimental section and listed in Table S1 of ESI.

- Gallic acid ($t_R = 12.2$ min), chlorogenic acid ($t_R = 22.6$ min) and eugenol ($t_R = 32.5$ min) were detected in the
- absorbance chromatogram at 280 nm (Figure 3 (a)). Tyrosol (t_R=19.3 min), catechin (t_R=20.4 min), (-
- 347)epicatechin (t_R =23.4 min), acetylsalycilic acid (t_R =27.5 min) oleuropein (t_R =30.2 min), and pinoresinol
- $(t_R = 32.5 \text{min})$ were identified using the fluorescence detector (Figure 3 (b)). Condensed water from CH
- 349 showed a similar phenolic profile.
- The condensed water, from IMWAE and CH, of clove buds is, thus, rich of bioactive compounds with well known, strong antioxidant properties (Pandey and Rizvi, 2009).
- 352 Among the different polyphenols detected, gallic acid, chlorogenic acid and eugenol were identified as
- the main compounds and their quantification is shown in Figure 3 (c) and 3 (d).

Figure 3

356

In the condensed water the composition of polyphenols showed small differences with respect to the 357 different extraction approaches employed (Figure 3 (c)). IMWAE yielded water extracts with almost one-358 third of eugenol than that obtained from CH. Since eugenol is the main compound of clove buds EO, and 359 the EO yield is higher using IMWAE, the residual lower concentration in the aqueous extracts can be 360 explained with its more effective MW-mediated extraction and separation from the aqueous extraction 361 mixture. This result agrees with the higher EO yield obtained by IMWAE (Figure 2 (a)). The concentration 362 of gallic acid in the condensed water obtained using microwaves (10.4 mg/g) was slightly lower than in 363 364 that from CH (13.9 mg/g). The amount of chlorogenic acid in the condensed water from IMWAE (1.9 mg/g) was comparable with that from CH (1.7 mg/g). 365

Figure 3 (d) shows the composition of hydrosoluble polyphenols extracted using different L/S_{ratio} by IMWAE. In agreement with the increase of EO yield as the L/S_{ratio} increases, the concentration of eugenol in the condensed water decreased as the L/S_{ratio} increased: eugenol was, indeed, distillated from the aqueous phase to the EO organic phase. However, in the cases of gallic acid and chlorogenic acid, the composition in the condensed water seems to have a maximum at L/S_{ratio}=20. The L/S_{ratio} during the IMWAE is an important factor to be controlled when the aim of the hydrodistillation is both the EO production and/or the polyphenols valorization.

Few works reported in the literature deal with the characterization and quantification of polyphenols 373 extracted from clove buds. Adefegha et al. reported the phenolic profile of the water obtained after cooking 374 clove buds and they quantified gallic acid, catechin, chlorogenic acid, caffeic acid, ellagic acid, rutin, 375 quercitrin, quercetin, kaempferol, and luteolin by HPLC-DAD analysis (Adefegha et al., 2016). The use 376 of solvents like methanol has been also investigated for the specific extraction of polyphenols from clove 377 buds (Dua et al., 2015). Gallic acid, eugenol, quercetin and tocopherol were identified in the methanol-378 water (80:20 v/v) extracts after 4 h of extraction at room temperature (Dua et al., 2015). The total amount 379 of polyphenols extracted was enhanced by the use of methanol. 380

The analysis of hydrosoluble polyphenols isolated in the condensed water after EO clove bud extraction has been limited to the total phenolic content assay (TPC) (Table 1). In this work, a qualitative and quantitative analysis of the condensed water obtained during clove buds EO isolation by both IMWAE and CH has been reported for the first time. In summary, the amount of hydrosoluble polyphenols, with strong antioxidant properties, found in the condensed water after the extraction of EO from clove buds, is significant and it opens new opportunities for condensed water valorisation.

388

389 FTIR-PLS analysis and thermal behavior of lignocellulosic residue

The solid residues remaining after the treatment of aromatic herbs aimed to extract EO represent the highest 390 mass of by-products after HD and it has been usually managed as waste, typically burned for energy 391 production (Kapadiya et al., 2018). This practice, however, is not efficient because of the high moisture 392 content of the solid residues, which leads to high costs of waste disposal. This type of solid residue is rich 393 394 of biopolymers like cellulose, lignin, hemicellulose, which represent a low-cost feedstock for biorefining. The depolymerization of lignocellulosic material into several feedstock chemicals such as glucose, 395 396 furfurals, levulinic acid and other compounds, is clearly a greener alternative (González-Rivera et al., 2014). However, its potential uses, as renewable feedstock, have been limited due to the scarcely available 397 information of its chemical composition. 398

Fourier Transform Infrared spectroscopy, thermogravimetric analysis and calorimetric combustion were 399 carried out in this work in order to characterize the solid residue after the IMWAE and CH. Figure 4 (a) 400 shows the FTIR spectra of raw dry clove buds and the corresponding extracted EO. The two spectra have 401 similar structural features due to the high amount of EO contained in the raw clove buds. The main peaks 402 observed match with the spectral profile of eugenol (OH stretching at 3516 cm⁻¹, symmetric and asymmetric 403 stretching of methylene and methyl groups at 2920 and 2853 cm⁻¹, CO bending at 1230 cm⁻¹, and C-C 404 stretching vibrations in the phenyl ring at 1640 cm⁻¹, 1514 cm⁻¹ and 1430 cm⁻¹), which is the main 405 compound in clove buds EO. Figure 4 (b) shows the FTIR spectra of the solid residues in the fingerprint 406 region (1900-800 cm⁻¹) after the IMWAE and CH. The intensity of the peaks corresponding to eugenol was 407 strongly reduced and two main peaks at 1618 and 1029 cm⁻¹ (C=O and C-O stretching vibrations of 408 cellulose and lignin) were observed. The solid residues of clove buds after both extraction processes showed 409 the characteristics of softwoods due to the peaks at 1316 cm⁻¹ (due to the condensation of guaiacyl unit and 410 syringyl unit, syringyl unit and CH₂ bending stretching) (Jiao et al., 2017), 1272 cm⁻¹ (guaiacyl ring 411 breathing and C=O stretching), 1160 cm⁻¹ (C-O-C stretching in pyranose rings, C=O stretching in aliphatic 412 groups) and 894 cm⁻¹ (due to cellulose P-chains and C-H stretching out of plane of aromatic ring) (Chen et 413 414 al., 2010).

416 Figure 4

417

The composition of cellulose, hemicellulose and lignin in the solid residue after EO extraction and raw 418 clove buds were predicted using a partial least square (PLS) model previously reported for the 419 determination of the chemical composition of hard and softwood samples (Chen et al., 2010). The PLS 420 model was reconstructed using the FTIR spectra of the wood samples in the region of 1900-800 cm⁻¹ (which 421 contains the fingerprint of wood components). The first derivative of the normalized FTIR spectra were 422 423 used as the X matrix and the chemical composition of lignin, cellulose and hemicellulose (determined by Van Soest analysis) as the Y matrix (Chen et al., 2010). The model was developed using JMP software and 424 7 principal components that explain the 98% of the variance in the X matrix and 98.8% of the variance in 425 the Y matrix (Chen et al., 2010). The prediction of the clove buds solid samples was then performed loading 426 their first derivative of the normalized FTIR spectra (Figure 5 (a)) into X matrix of the model and the cross-427 validation technique was applied. Figure 5 (b) reports the comparison of the predicted chemical 428 composition in terms of cellulose, hemicellulose and lignin in raw clove buds and in the dry solid residue 429 after IMWAE or CH EO extraction. 430

431

432 Figure 5

433

The PLS predicted chemical composition of raw clove buds indicate that hemicellulose (26 %), cellulose (19 %) and lignin (37%) represent about 80%. The mass balance is reached considering about 15.4 - 16.1% volatile compounds (which include EO and 4-5% water determined by TGA under nitrogen flow (step 1 of weight loss in Table 3 below) and 5% inorganic materials (determined as ash by TGA under oxygen flow).

The PLS predicted chemical composition of dry solid residue after IMWAE or CH EO extraction (Table 2) evidenced that the three different components account for 78 and 80 % in the mass balance, respectively. Considering that about 6% is due to volatile compounds determined by TGA under nitrogen flow (step 1 in Table 3 below) and less than 4% is due to inorganic material in both, it can be hypothesized that the missing part to the mass balance (about 12% and 10% in IMWAE and CH dry residue, respectively) is due to a partial loss of lignin (Kang et al., 2013; Toledano et al., 2014).

445 **Table 2**

446

Interestingly, lignin apparently decreases, and cellulose apparently increases in dry residues depending on 447 the thermal treatment that characterizes the respective extraction method, and this is more enhanced in solid 448 residues after IMWAE extraction (Table 2). This result is not surprising considering that microwaves may 449 promote a partial degradation of lignin or other wood components (e.g. hemicellulose or cellulose), 450 suggesting a higher interaction of phenolic compounds with microwaves, thus giving higher EO yields. In 451 the specific case, the apparent increase of cellulose may be due to a bias of the PLS model based on the van 452 Soest extraction of whole, untreated woods (Chen et al., 2010). Following the hypothesis above, the 453 insoluble part derived from lignin degradation may interfere with the quantitation of cellulose. 454 Hemicellulose percentage in the solid residue from CH (24 %) was comparable with that contained in raw 455 456 clove buds (25 %) and slightly higher than that found in the residue after IMWAE (20 %).

Figure 6 shows the thermograms related to the pyrolysis of clove buds and the solid residues from IMWAE
and CH extractions and Table 3, summarizes the experimental temperatures and percentage mass losses of
the corresponding degradation steps.

460

461 Figure 6

462

Four different mass losses were identified during the thermal analysis of clove buds and the solid residues from IMWAE and CH extractions. The mass loss below 150 °C is related to the essential oil evaporation in raw clove buds (15.4% at $T_{peak}=95$ °C) and to moisture evaporation (almost 6% at $T_{peak}=50$ °C) in solid residues from IMWAE and CH. The mass losses above 150 °C are due to the solid portion of the samples, and they have been assigned in the literature to the pyrolysis of lignocellulosic materials: hemicellulose in the temperature range 215-220 °C, cellulose in the temperature range 315-400 °C and lignin in the temperature range 160-900 °C (Carrier et al., 2011; Sher et al., 2020; Yang et al., 2007).

470

471 **Table 3**

472

The pyrolytic profiles of the solid residues from IMWAE and CH extractions are identical among them and slightly different to that of raw clove buds. To directly compare the mass losses of lignocellulosic materials of the solid residues from IMWAE and CH extractions to those of raw clove buds the curves have been 476 rescaled by taking the value at 150 °C as 100%, thus eliminating the mass losses due to essential oil and 477 moisture evaporation. The rescaled mass losses are reported in Table S2 of ESI. The mass losses in the 478 temperature range 150-400 °C highlight a significant decrease (2-3 times) of the hemicellulose/cellulose 479 ratio in both residues respect to raw clove buds, in agreement with PLS data.

Figure 7 shows the profiles of the main gaseous products obtained by monitoring their strongest IR bands (CO2 λ =2371 cm⁻¹, CO λ =2165 cm⁻¹, small-oxygenated compounds λ =1738 cm⁻¹ and methane λ =3015 cm⁻¹ evolved during the thermal decomposition of residues after IMWAE (a) and CH (b).

Figure S1 shows the results of TG-FTIR analysis at three significant temperatures (T= 240 °C, 345 °C and 484 490 °C). The FTIR spectra showed that both IMWAE and CH solid residues evolve similar gases at T=240 485 °C, i.e. CO₂ (2358, 2322 cm⁻¹ O=C=O asymmetric stretching and, 668 cm⁻¹ O=C=O bending), CO (2181, 486 2106 cm⁻¹ stretching), H₂O (3736 cm⁻¹ OH symmetric stretching) and small oxygenated compounds 487 (aldehydes and carboxylic acids, 1738 cm⁻¹ C=O stretching, 2930 cm⁻¹ -CH₂- stretching, 2859 cm⁻¹ –CH 488 symmetric stretching and methane (3015 cm⁻¹ C–H stretching).

It has been reported that CO₂ evolution during lignocellulosic thermal degradation is due to the cracking 489 490 and reforming of functional groups of carboxyl (C=O) and COOH (Yang et al., 2007). CO₂ is released at all three different temperatures explored (matching with the hemicellulose, cellulose and lignin degradation 491 492 steps). The intensity of CO_2 signal was higher at lower temperature. The CO_2 production during lignocellulosic material degradation is, indeed, associated to hemicellulose degradation (due to its higher 493 494 carbonyl content units) (Yang et al., 2007). CO was evolved at higher temperature with two remarkable peaks at 350 and 500 °C (Figure 7). The evolution of CO was mainly related to cellulose decomposition 495 due to the high carbonyl units contained in the cellulose polymer. Lignin decomposition can be observed 496 by following the methane evolution profile. CH₄ evolved mainly after 500 °C due to the thermal cracking 497 of methyl groups contained in lignin (Methoxyl-O-CH₃) (Yang et al., 2007). Thus, the evolution profiles 498 of gases allowed us to identify the three main decomposition steps related to hemicellulose, cellulose and 499 lignin, respectively. 500

501

502 **Figure 7**

503

The CO₂ evolution profiles of Figure 7 have different intensity in solid residues obtained after IMWAE and CH. Under the same experimental conditions, the differences in the IR intensity could indicate different

concentration of the gas evolved (Yang et al., 2007). The comparison between the IR intensity of CO₂ 506 signals observed in the evolution profile of solid residues from IMWAE highlighted that the peak with a 507 maximum value at 345 °C (due to the main cellulose decomposition) and the two peaks with lower IR 508 intensity at 240 °C and at 660 °C (due to hemicellulose and lignin decomposition, respectively) correspond 509 to a solid residue with lower amount of hemicellulose and lignin, respectively. A similar behaviour of the 510 IR intensity of CO₂ signals was observed in the evolution profile of solid residues from CH. However, the 511 intensity of all peaks was lower than that observed in the residue from IMWAE (Figure 7(b)). It can be 512 hypothesized that MW irradiation produce a solid residue characterized by the increase of branched 513 hemicellulose hydrolysis and, thus, an enhancement of phenolic compounds extraction (EO and lignin). 514 This effect is expected also during CH but it is more evident in IMWAE due to the acceleration of the 515 516 extraction process.

517 A further characterisation of the solid residues from IMWAE and CH, using their corresponding pyrolytic 518 profiles obtained by the non-isothermal thermogravimetric analysis, is in progress through the biomass 519 pyrolysis kinetics investigation.

In the prospective biorefining of clove buds according to Figure 1 the calorimetric combustion of IMWAE and CH residues were determined in order to assess the enthalpy of combustion values (Δ_c H). This information is useful for the alternative uses of solid residues as fuels for energy production.

The standard enthalpy of combustion ($\Delta_c H^\circ$) of the solid residues from IMWAE and CH was calculated 523 using the standard enthalpy of formation ($\Delta_f H^\circ$) reported for hemicellulose, cellulose and lignin 524 components (Gorensek et al., 2019). The biomasses derivate from clove buds showed characteristics of 525 softwoods (Chen et al., 2010), the $\Delta_f H^{\circ}$ and monomer units for the three components were then selected 526 accordingly: hemicellulose (monomer xylose units, MW = 132.12 g mol⁻¹, $\Delta_f H^\circ = -759.2$ kJ mol⁻¹), 527 cellulose (monomer glucose unit, MW = 161.14 g mol⁻¹, $\Delta_f H^\circ = -1019.0$ kJ mol⁻¹) and lignin (monomer 528 unit, MW = 258.27 g mol⁻¹, $\Delta_f H^\circ = -759.39$ kJ mol⁻¹) (Gorensek et al., 2019). The $\Delta_c H^\circ(i)$ values were 529 calculated by Eq. (2): 530

531
$$\Delta_{c}H^{\circ}(i) = \nu_{CO_{2}}\Delta_{f}H^{\circ}_{CO_{2}} + \nu_{H_{2}O}\Delta_{f}H^{\circ}_{H_{2}O} - \Delta_{f}H^{\circ}(i)$$
(2)

532 (i = hemicellulose, cellulose, lignin)

- 534 Where $\Delta_{\rm f} {\rm H}^{\circ} {\rm CO}_2 = -393.51 \, {\rm kJ \ mol^{-1}}$ and $\Delta_{\rm f} {\rm H}^{\circ} {\rm H}_2 {\rm O} = -285.83 \, {\rm kJ \ mol^{-1}}$ are the standard enthalpies of formation 535 of carbon dioxide and liquid water, respectively and vCO₂ and vH₂O are the stoichiometric coefficients of 536 CO₂ and H₂O in each combustion reaction:
- 537 Hemicellulose: $C_5H_8O_4 + 5O_2 \rightarrow 5CO_2 + 4H_2O_3$
- 538 *Cellulose*: $C_6H_{10}O_5 + 6O_2 \rightarrow 6CO_2 + 5H_2O$

539 Lignin:
$$C_{15}H_{14}O_4 + 33(\frac{1}{2})O_2 \rightarrow 15CO_2 + 7H_2O_4$$

540 The combustion enthalpy values calculated by Eq. (2) for hemicellulose, cellulose and lignin are 541 $\Delta_c H^{\circ}hemi = -2351.67 \text{ kJ mol}^{-1}, \Delta_c H^{\circ}cell = -2771.21 \text{ kJ mol}^{-1}$ and $\Delta_c H^{\circ}lig = -7144.07 \text{ kJ mol}^{-1}$.

From the known values of the percentage compositions in hemicellulose cellulose, and lignin, assumed asto be the only burning components, the combustion enthalpy of the biomass can then be calculated:

544
$$\Delta_c H_{biomass}/kJ g^{-1} = \frac{\sum_{i=1}^{3} (\%_i \frac{\Delta_c H_i^{\circ}/kJ mol^{-1}}{MW_i/gmol^{-1}})}{100}$$
 (3)

545

546 (i = hemicellulose, cellulose, lignin)

Table 4 shows the Δ_c H for solid residues from IMWAE and CH calculated from the percentage composition of Table 2 (obtained by FTIR chemometrics) according to Eq. (3) compared with experimental values obtained by direct calorimetry and with the higher heating value reported for solid residues from clove buds treated with a MW process (Kapadiya et al., 2018). Two different values were calculated for each sample from the percentages of FTIR PLS analysis data.

The first value is calculated considering only the lignin content found with the chemometric method as is, therefore, is expected to be underestimated. The second value considers the total lignin, that is also the degraded fraction missed by PLS analysis, by attributing to it the same heat of combustion as lignin. The latter value is therefore expected to be overestimated.

Thus, the enthalpy of combustion of the solid residue from IMWAE should be between -15.40 and -18.41 kJ g⁻¹ and that from CH should be between -16.60 and -19.00 kJ g⁻¹. This is consistent with the experimental values.

560 **Table 4**

561

The experimental $-\Delta_c H$ (kJ g⁻¹) values of solid residues from IMWAE and CH (Table 4) are in line with those reported for lignocellulose woods (i.e. pine ($-\Delta_c H=20.68$ kJ g⁻¹), spruce ($-\Delta_c H=20.5$ kJ g⁻¹), poplar ($-\Delta_c H=19.57$ kJ g⁻¹), bagasse ($-\Delta_c H=18.82$ kJ g⁻¹), corn stalks ($-\Delta_c H=18.60$ kJ g⁻¹), sweetgrass ($-\Delta_c H=18.66$ kJ g⁻¹), wheat straw($-\Delta_c H=18.43$ kJ g⁻¹)) (Ioelovich, 2018). The calculated $-\Delta_c H$ (kJ g⁻¹) using the composition predicted by PLS of FTIR spectra are in a reasonable agreement with the experimental values and the HHV reported. The $\Delta_c H$ highlights the energetic features of solid residues from IMWAE and CH for their potential uses as alternative biomass for fuel production.

569 Conclusions

570

Full valorization of aromatic herbs through an energy efficient and eco-friendly approaches addresses well
the goals of the agenda 2030 for sustainable development of the United Nations (Marco et al., 2020).

The chemical characterization of the three products obtained after IMWAE of clove buds and the 573 quantification of their main components (EOs, polyphenols in the condensed water and solid residue) 574 proposed in this work represents an essential step for their further valorization and exploitation. Moreover, 575 the IMWAE here proposed represents a green, competitive and economically attractive approach easily 576 applicable to a wide gamma of different substrates like aromatic herbs, spices and seeds and it may suggest 577 how to increase the shareholder value, and to maximize the profit of these novel hydrodistillation processes 578 (Gonzalez Rivera et al., 2016; Santana-Méridas et al., 2014), in agreement with the concept of biorefinery 579 and sustainable chemistry (Corona et al., 2018; Gonzalez-Rivera et al., 2016; Rombaut et al., 2014). 580

IMWAE has the following technological advantages: i) the use of several independent coaxial antennas applied in situ should permit to extend MW irradiation to very large batch reactors (pilot plants) as well as to continuous flow systems (production scale); (ii) any problem due to high processable volumes is in principle overcome because the method offers the possibility of breaking the scale-up and scale-out barrier in industrial processes, enabling a better control of the local temperature and of its distribution, in comparison with other microwave systems commonly employed; (iii) due to its versatility, this method can be applied to most of the process technologies already available; (iv) the proposed microwave extractor is not a resonant cavity applicator, so that it is apart from the conventional definition and differentiation
between multi-mode and mono-mode conventional microwave instruments.

590 Unimportantly, the biorefining of clove bud components, well known for their antiviral effect can open new 591 opportunities for the exploitation and application of low cost, worldwide available and naturally-occurring 592 antivirals to the treatment of current and future outbreak pandemic emergences.

593

594 **Credit authorship contribution statement**

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Emilia Bramanti: Conceptualization, Methodology, Investigation. José Gonzalez-Rivera, Celia Duce, Luca
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601 **Declaration of Competing Interest**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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TABLES

Table 1. Literature reports of clove buds extracts isolated by different approaches and comparison with the IMWAE developed in this

848 work.

		Extraction conditions			Characterizati	on of extracts										
Approach	Source		S/L ratio	in	EO	EO Hudro			Ref.							
Approach	Source	Time, min	(w/w)	Solvent	Yield % (wt)	Main compounds (%)	 Hydrosoluble Polyphenols (mg/g) 	Solid residue analysis	Ker.							
IMWAE	Indonesia	90 1 1:40 120		1:40 H ₂ O		1:40 H ₂ O	1:40 H ₂ O		1:40 H ₂ O		1:40 H ₂ O	16	eugenol (48.9) β -caryophyllene (42.8) α -caryophyllene (3.7)	Gallic acid (10.4) Chlorogenic acid (1.9) Eugenol (10.4)	FTIR (PLS model)Hemicellulose 20 ± 1 %Cellulose $40\pm4\%$ Lignin $30\pm3\%$ $-\Delta_c H= 17.07^a$ FTIR (PLS model)	This work
СН					7.8	eugenol (49.2) β -caryophyllene (43.5) α -caryophyllene (3.8)	Gallic acid (13.9) Chlorogenic acid (1.7) Eugenol (33.5)	Hemicellulose $24\pm1\%$ Cellulose $31\pm3\%$ Lignin $34\pm4\%$ $-\Delta_cH=17.62^a$								
IMWAE	Madagascar	120	1:5	H ₂ O	5.9	eugenol (66.9) β -caryophyllene (24.8) α -humulene (3.1) eugenel (87.1)	no	no	(Gonzalez Rivera							
СН		360			9.7	eugenol (87.1) eugenyl acetate (6.4) β-caryophyllene (5.1) eugenol (81.1)			et al., 2016)							
SD		240	1:20	Steam	18.2	eugenyl acetate (18.1) α –caryophyllene (0.7) eugenol (76.8)										
Soxhlet		1440		CH_2Cl_2	17.4	eugenyl acetate (15.2) β-caryophyllene (7.9)										
SHWE	Madagascar	100		Superh eated water (150°C)	18.3	eugenol (83.6) eugenyl acetate (16.1) β-caryophyllene (1.0)	no	no	(Clifford et al., 1999)							
SFE		200 bar-55	°C-330 min	SC- CO ₂	21.5	eugenol (76.2) eugenyl acetate (15.7) β-caryophyllene (8.1)										
MAE CH	India ^b	30 180	1:6.7 1:25	H ₂ O	13.1 12.5	eugenol (90.1) eugenol (88.1)	TPC of hydrosol (83.58 mg GAE/g)	Proposed as alternative source of fuel(i.e. coal)	(Kapadiya et al., 2018)							

MAE		80	H ₂ O	13.9	eugenol (88.8) eugenyl acetate (7.5)			
WIAL		50	1120	15.7	β -caryophyllene (2.7) eugenol (83.4)			
MASE	Iran ^b	80 1:10	steam	12.7	eugenyl acetate (14.3) β -caryophyllene (1.4)	no	no	(Golmakani et al.,
СН		240	H ₂ O	13.0	eugenol (87.3) eugenyl acetate (10.4) β -caryophyllene (1.4)			2017)
SD		240	steam	11.5	eugenol (82.7) eugenyl acetate (15.6) β -caryophyllene (0.9)			
MWHD		40 1:1	H ₂ O	3.2	eugenol (65.2) β-caryophyllene (12.1)	no	no	(Leon-méndez et
СН		180	1120	2.9	eugenol (60.3) β-caryophyllene (11.6)	10	10	al., 2018)
SFE		90 bar-50°C	SC- CO ₂	20.8	eugenol (65.9) eugenyl acetate (19.0) β-caryophyllene (11.1)	no	no	(Reverchon and Marrone, 1997)
SFE		100 bar-50°C-120 min	SC- CO ₂	19.6	eugenol (58.8) eugenyl acetate (19.6) β-caryophyllene (14.0) eugenol (58.2)			
SD	China ^b	600 1:5	steam	10.1	β-caryophyllene (20.6) eugenyl acetate (13.8)	no	no	(Guan et al., 2007)
СН		360	H ₂ O	11.5	eugenol (48.8) β -caryophyllene (36.9) α -humulene (4.4)			
Soxhlet		360 1:8.3	Ethanol	41.8	eugenol (57.2) eugenyl acetate (19.4) β-caryophyllene (17.5)			
SFE		90 bar-40°C-240 min	SC- CO ₂	14.2	eugenol (63.5) eugenyl acetate (18.8) β-caryophyllene (13.7)	no	no	(Scopel et al., 2014)
US-SFE	Taiwan ^b	150 bar-40°C-115 min	SC- CO ₂	22.1	eugenol (59.2) eugenyl acetate (18.6) β-caryophyllene (15.4)	no	no	(Yang et al., 2014)

are		200.1	1000 170 :		10.1	eugenol (55.6)			
SFE	200 bar-40°C-170 min			19.1	eugenyl acetate (17.1)				
						β -caryophyllene (14.5) eugenol (34.1)			
SE		360	1:20	Hexane	17.5	eugenyl acetate (10.5)			
						β -caryophyllene (9.1)			
						α -humulene (\approx 32)			
	India				41	eugenol (≈8)			
				F (1 1		eugenyl acetate (≈ 5)			
UAE	China	45	1:20	Ethanol : H2O	41	α-humulene (\approx 45) eugenol (\approx 9)	TPC of crude extracts $(101 + 1 \text{ to } 215 + 3 \text{ mg})$	20	(Alexandru et al.,
	China	43	1:20	(1:1)	41	eugenyl acetate (≈ 8)	$(191 \pm 1 \text{ to } 215 \pm 3 \text{ mg})$ GAE/L)	no	2013)
				(1.1)		α -humulene (≈ 26)	$O(\mathbf{E}, \mathbf{E})$		
	Madagascar				39	eugenol (≈9)			
	-					β -caryophyllene(\approx 5)			
UAE	Turkey ^b	45	1:20	Ethanol	28.2	eugenol (64)	no	no	(Tekin et al.,
						α -caryophyllene (n.r.)			2015)

851 MWHD=microwave assisted hydrodistillation; CH=hydrodistillation; MAE=microwave assisted extraction; SFE=Supercritical fluid extraction;

852 MASD=microwave-assisted steam distillation; US-SFE=ultrasound-assisted supercritical fluid extraction, UAE=ultrasound assisted extraction;

853 SD=steam distillation; SE=solvent extraction; SHWE=superheated water extraction. S/L=solid/liquid. ^a Experimental enthalpy of combustion

854 (kJ/g); ^b clove buds purchased from local market in the country stated; the native production of the plant is not mentioned.

Table 2. PLS predicted chemical composition of cellulose, hemicellulose and lignin in dry solid residue
after the IMWAE and CH (N= 3 replicates).

	PLS %				
components	Raw clove buds	Solid residues after extraction			
	Kaw clove buds	IMWAE	СН		
Hemicellulose	25±5	20±1	24±1		
Cellulose	19±2	40±4	31±3		
Lignin	37±6	18±3	25±4		
Insoluble "degraded" lignin ^a	-	12	10		
Total lignin	37±6	30±3	35±4		
Moisture and volatiles ^b	15±2	6±2	6±2		
Ash ^c	5 ±2	2±2	2±2		

861 IMWAE= In situ microwave assisted extraction; CH=hydrodistillation. ^a Calculated by difference; ^b step

862 (I) Table 3 TGA under nitrogen flow; ^c TGA under air flow.

8	6	7	

868	Table 3. Experimental temperatures and percentage mass losses of the corresponding degradation steps
869	under nitrogen flow of raw clove buds and solid residues from IMWAE and CH extractions.

	Mass loss/wt % ($(T_{peak}/^{\circ}C)$	peak/°C)		
Step	Raw clove buds	Solid residues after extraction			
	Kaw clove buus	IMWAE	СН		
Ι	15.4	5.9	6.1		
Volatiles (<150 °C)	(95)	(53)	(52)		
П	15.0	10.5	11.0		
	(220)	(235)	(236)		
Main degradation of hemicellulose and cellulose (150-400 °C)	27.9	40.6	39.3		
(130-400 C)	(327)	(340)	(338)		
III	17.1	19.9	20.3		
Main degradation of lignin	(405, 460, 632)	(407, 485, 632)	(407, 485, 632)		
(400-800 °C)	(403, 400, 032)	(407, 403, 032)	(407, 403, 032)		
Residual mass	24.6	23.1	23.3		
at 900 °C	24.0	23.1	23.3		

871 IMWAE= In situ microwave assisted extraction; CH=hydrodistillation.

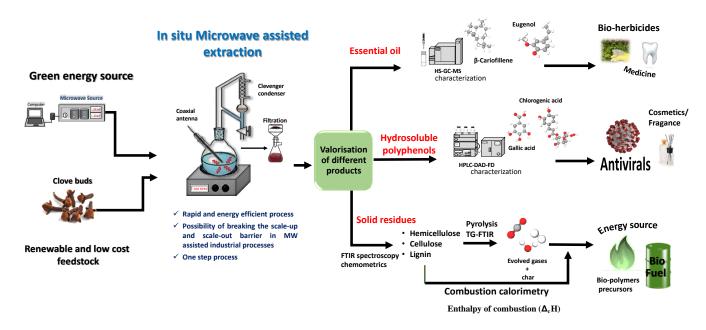
Table 4. Δ_c H for solid residues from IMWAE and CH.

	$-\Delta_{c}H$ (kJ/g)		
Estimation method	solid residue from IMWAE	solid residue from CH	Reference
FTIR chemometrics	15.40 ^a 18.41 ^b	16.60 ^a 19.00 ^b	This work
Experimental Combustion calorimetry	17.07	17.62	This work
Higher heating value	21.1758		(Kapadiya et al., 2018)

880 IMWAE= In situ microwave assisted extraction; CH=hydrodistillation; Δ_c H= enthalpy of combustion. ^a 881 Calculated considering only the lignin content found with the chemometric method; ^b Calculate accounting 882 also for "degraded" lignin (see text).







890

Figure 1. Overview of the herein studied approach for the isolation and characterization of different extracts from clove buds by IMWAE and its potential for biorefining. HS-GCMS=Head space gas chromatography mass spectrometry; HPLC-DAD-FD=High performance liquid chromatography with diode array detector and fluorescence detector; TG-FTIR=thermogravimetric analysis coupled to Fourier transform infrared spectroscopy; Δ_c H= enthalpy of combustion.

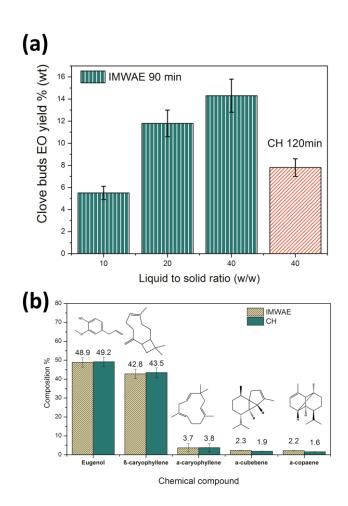


Figure 2. (a) Yield mass % of EO extracted from clove buds by IMWAE at different liquid to solid ratio.
(b) Chemical composition of clove buds EO obtained by IMWAE (liquid to solid ratio=40) and CH (liquid to solid ratio=40). Extraction conditions: MW applied power 150W at 2.54 GHz, clove buds from Indonesia and water as solvent, extraction time (90 min of IMWAE and 120 min of CH, N=3 replicates). IMWAE=
In situ microwave assisted extraction; CH=hydrodistillation; EO=essential oil.



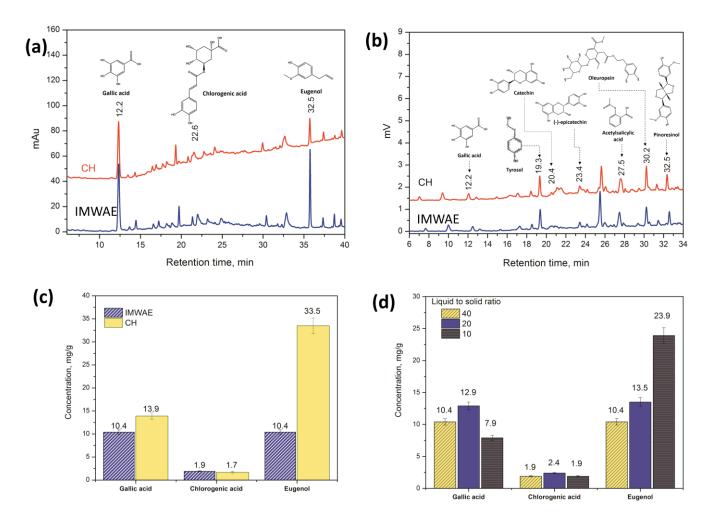


Figure 3. Polyphenols profile detected by HPLC-DAD-FD: (a) absorbance chromatogram at 280 nm, (b)
fluorescence chromatogram of clove buds condensed water from IMWAE (blue line) and CH (red line) and
(c) the main hydrosoluble polyphenols simultaneously quantified in condensed water after the extraction
of EO from clove buds by IMWAE and CH. (d) Effect of clove bud amount (L/S_{ratio}) during IMWAE.
Extraction conditions: 90 min of MW irradiation at 2.54 GHz. IMWAE= In situ microwave assisted
extraction; CH=hydrodistillation; EO=essential oil.

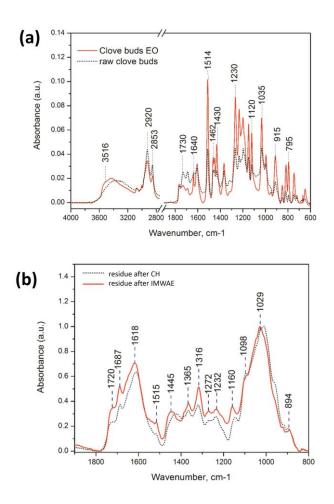


Figure 4. (a) ATR-FTIR spectra of clove buds EO and the raw clove buds. (b) ATR-FTIR spectra of the
solid residue after IMWAE and CH. IMWAE= In situ microwave assisted extraction; CH=hydrodistillation;
EO=essential oil.

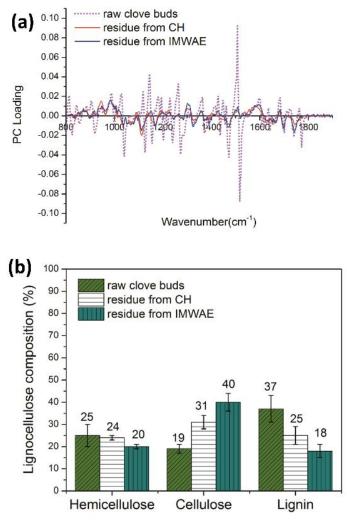


Figure 5. (a) Loadings profile (first derivative) of solid residue for the cross-validation-PLS prediction
model. (b) PLS predicted chemical composition of cellulose, hemicellulose and lignin in dry solid residue
after the IMWAE and CH (N= 3 replicates). IMWAE= In situ microwave assisted extraction;
CH=hydrodistillation.

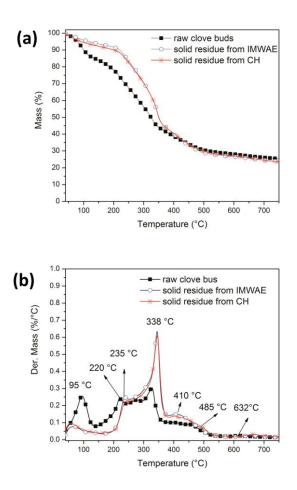


Figure 6. TG curves (a) and DTG curves (b) under nitrogen flow for the raw clove buds and solid residues
from IMWAE and CH extractions. IMWAE= In situ microwave assisted extraction; CH=hydrodistillation;
EO=essential oil.

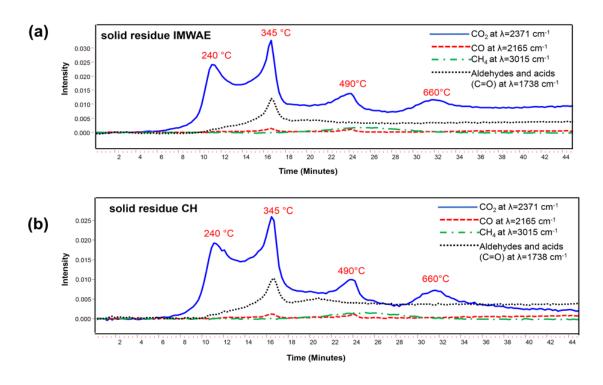


Figure 7. Evolution profiles of gases evolved from the TG-FTIR analysis of clove bud solid residues after
IMWAE (a) and CH (b) (thermal decomposition at 20 °C min under N₂). IMWAE= In situ microwave
assisted extraction; CH=hydrodistillation; EO=essential oil.